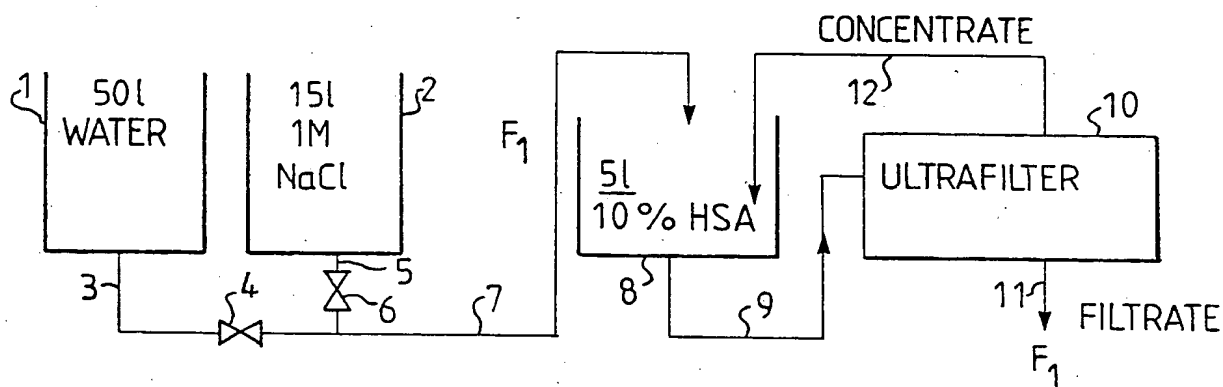




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(21) International Application Number: PCT/SE90/00442 (22) International Filing Date: 20 June 1990 (20.06.90) (30) Priority data: 8902317-0 27 June 1989 (27.06.89) SE (71) Applicant (for all designated States except US): KABIVITRUM AB [SE/SE]; S-112 87 Stockholm (SE). (72) Inventor; and (75) Inventor/Applicant (for US only) : EKETORP, Rainer [SE/SE]; Noragårdsvägen 56, S-182 34 Danderyd (SE). (74) Agents: ONN, Thorsten et al.; AB Stockholms Patentbyrå Zacco & Bruhn, Box 3129, S-103 62 Stockholm (SE).		(81) Designated States: AT (European patent), AU, BE (European patent), CA, CH (European patent), DE (European patent)*, DK (European patent), ES (European patent), FI, FR (European patent), GB (European patent), IT (European patent), JP, LU (European patent), NL (European patent), NO, SE (European patent), US. Published <i>With international search report.</i> <i>With amended claims.</i>

(54) Title: METHOD OF CLEANSING PROTEINS**(57) Abstract**

The invention relates to a method of cleansing a protein from multivalent metal ions bound thereto, these ions being released from the protein by exchanging the ions with monovalent metal ions, whereafter the multivalent metal ions are removed. The release and removal of these ions is effected, in particular, by diafiltration or gel filtration processes.

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METHOD OF CLEANSING PROTEINS

The present invention relates to a method of cleansing protein from multivalent metal ions bound thereto.

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Many biologically active proteins have obtained wide use as important drugs. As a result primarily of different cleaning methods, these proteins are liable to contain relatively large quantities of different metals. An investigation into the proportions of metals in various biological products was published in 1986 (6), and it is evident from this investigation that the proportions of metals in, for instance, human serum albumin can reach values which are harmful to patients.

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The metals normally derive from the various additives used when working-up and cleansing the proteins. For instance, these processes normally involve the use of filter aids and filters having a relatively high proportion of filter aids for the purpose of clear-filtering solutions in various process stages. These filter aids have often been found to contain metals which are able to bind to the protein in ion form. The problems can be overcome by using other filtering methods, using filters based on inert materials. Such filters, however, are at present particularly expensive in comparison with the filter materials conventionally used.

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In the case of many proteins, multivalent metal ions are bound strongly to the protein, probably due to chelate formation and ion-exchange effects.

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Endeavours have also been made to remove the bound metals ions by treatment with various complex formers,

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such as EDTA or citrate ions. The metal ions, however, are bound so strongly to the proteins that these endeavours have met with no success.

5 The contaminating multivalent metal ions in the proteins may, for instance, consist of one or more of the metals aluminium, chromium, lead, mercury, iron, nickel, copper and magnesium. Of these metal ions, the removal of aluminium, iron and lead is the most important.
10

Aluminium, which is the most common metal in the earth's crust has been assumed to constitute an ethiological factor in a number of clinical illness conditions, such as senile demens of the Alzheimer type (1, 15 2) and dialysis encephalopath (3, 4, 5), etc. It has been clearly established that aluminium is accumulated in the tissues and has a toxic effect on patients suffering from kidney function disorders.
20

The injurious effect of other metals, such as iron, chromium, nickel and lead, is previously known, either due to their normal toxicity, or due to their ability to promote allergies, for instance.
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The aforesaid disadvantages are avoided by the present invention, which provides a method of cleansing proteins of the multivalent metal ions bound thereto, so as to obtain as the end product one or more proteins in which the proportion of strongly bound multivalent metal ions is greatly reduced.
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In accordance with the present invention, a protein is cleansed of multivalent metal ions bound thereto by releasing the multivalent metal ions by exchanging said
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multivalent ions with monovalent metal ions and removing the replaced multivalent metal ions. In accordance with one particular embodiment of the invention, the monovalent metal ions are subsequently also removed.

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The monovalent metal ions used to substitute the multivalent metal ions are primarily alkali metal cations, and then particularly sodium or potassium, or ammonium cations.

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The accompanying drawing is a flow sheet of a diafiltration process, which constitutes one embodiment of the invention and which is described in more detail in the following examples.

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The multivalent metal ions bound to the protein are exchanged with the monovalent metal ions, by treating a solution of the protein with a solution of a salt of a monovalent metal ion in high concentration. This process displaces the equilibrium, so that the multivalent cations are displaced by the monovalent cations. The released multivalent metal cations can then be removed with the aid of one or several known processes. Processes found particularly operable in both exchange stages are diafiltration and gel filtration.

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In the case of diafiltration, the liquid to be filtered is caused to flow parallel with the surface of the filter and a pressure gradient is applied over the filter. The pore size of the filter is selected in correspondence with the molecular size of the protein to be cleansed, so that the protein molecules are retained while the metal ions pass through the filter. The size of the pores is normally of the order of nanometers. A solution of salt of monovalent metal ions in

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high concentration is added to the protein solution, before passing the solution over the filter surface. This causes the bound multivalent metal ions to be displaced from the protein and substituted by monovalent metal ions, and the multivalent metal ions will then pass through the filter as filtrate. A further solution of monovalent metal salt in a quantity corresponding to the withdrawn filtrate is then added to the resultant protein-solution concentrate, and the solution is recycled for further filtration, this process being continued until the content of multivalent metal ions has been reduced to the desired value.

If desired, the diafiltration process can then be continued with the addition of water instead of salt solution, the monovalent metal ions being displaced from the protein molecules and removed through the filter.

The same principles can be applied in gel filtration, using some known gel filtration material, e.g. a cross-linked dextran gel, such as Sephadex[®] G 10 or G 25. The gel filter material is selected so as to have an appropriate pore size commensurate with the molecular size of the protein to be cleansed. The gel filtration process is carried out with the protein in a buffer solution containing a high proportion of monovalent metal salt, in order to displace the bound multivalent metal ions. The desired cleansing effect can be achieved, in the majority of cases, by adding a sufficient quantity of monovalent metal salt to the sample to be gel-filtered. When the pore size of the gel-filter material is correctly adapted, the protein will flow through the filter medium while the multivalent metal ions will be delayed, thereby enabling said multivalent metal ions to be isolated from the protein.

The proportion of monovalent metal salt in the solution used to displace the multivalent metal ions from the protein in the diafiltration or gel filtration process can vary within relatively wide limits. The absolute lowest limit of this range is determined by the physiological salt content, thus 0.9% w/v or 0.15 M. The upper limit is decided, in principle, by the saturation content of the salt concerned in the solution, although other factors may also have significance. For instance, some proteins can be denatured by high salt contents. The person skilled in this art, however, will have no difficulty in finding an operable salt content on the basis of simple experiments.

Particularly different types of proteins can be cleansed by means of the inventive method. The method has been found particularly expedient for cleansing albumin, such as human serum albumin, and gammaglobulin. The invention is not restricted, however, to the cleansing of solely these proteins.

The invention will now be further illustrated with reference to the following examples.

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Example 1:

5 l of a 10-percent solution of human serum albumin (HSA) was diafiltered against 15 l of a 1M sodium chloride solution. Apparatus for carrying out the method are shown schematically in the accompanying drawing.

The apparatus include a water storage tank 1 and a supply tank 2 for 1M sodium chloride solution. The storage tanks are connected to a common conduit 7 which leads to a storage container 8 for albumin solution,

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via outlet pipes 3 and 5 and valves 4 and 6 respectively. The albumin solution is passed from the container 8 through a pipe 9 and into an ultra-filtering device 10, the filter of which has a porosity of 10 000 ("cut off" molecular weight). A filtrate is removed from the filter device 10 through a pipe 11 and a concentrate is recirculated through a pipe 12 to the storage vessel 8. The removed filtrate has a volume of F_1 , and an equally large volume F_1 of water or salt solution is passed to the storage vessel 8, through the pipe 7, so as to hold the volume constant.

During the filtration process, the valve 4 is closed and the valve 6 open at first, and salt solution is passed from the storage tank 2 to the storage container 8, so as to displace the multivalent metal ions from the protein, these multivalent metal ions then being removed in the filtrate, through the pipe 11. When the filtration process has continued over a length of time such that the proportion of multivalent metal ions in the protein has been reduced to the desired value, the valve 6 is closed and the valve 4 opened, and the filtration process is continued with the addition of clean water, so as to, in turn, displace the monovalent metal ions from the protein and remove said monovalent ions in the filtrate, through the pipe 11. Filtration with the addition of clean water is then continued until the proportion of monovalent metal ions has decreased to the desired value.

In the illustrated example, 15 l 1M sodium chloride solution is added continuously to the albumin solution during the filtering process, wherewith the proportion of multivalent metal ions in the albumin solution, e.g. aluminium, is reduced to a value beneath 30 $\mu\text{g/l}$. The

input values of the metal content normally lie within the range of 200 to 1500 $\mu\text{g/l}$. The reduction of the proportion of undesirable multivalent metal ions in the protein is thus very considerable.

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The proportions of Fe, Pb and Cr in the input albumin solution were 3.2, 0.36 and 0.6 mg/l respectively. Subsequent to treatment, these proportions were found to have reduced to 0.3, 0.08 and 0.02 mg/ml respectively.

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Example 2:

Crude albumin from ethanol fractionation of plasma (Fr. V) was dissolved to a content of about 10% in distilled water. The solution was filtered and the pH adjusted to 7.0.

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Diafiltration was then effected against a sodium chloride solution, containing 2 mol/l NaCl. 135 l of this solution was used in total. For each 45 liters added, samples were taken for determining the aluminium content. Ultrafilters having a "cut off" of 10 000 were used. The results are set forth in the following Table 1:

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Table 1

Diafiltration solution added	Al-content mg/l
0	0.35
45	0.16
90	0.11
135	0.04

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Subsequent to reducing the sodium content, the aluminium content was found to be 0.01 mg/l.

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Example 3:

Crude albumin according to Example 2 was dissolved in distilled water to a proportion of about 10%. The solution was filtered and the pH of the filtrate adjusted to 7.0. The total volume was 3 liters. Solid sodium chloride was added to the solution, to a proportion of 2 mol/l, and the aluminium proportion of the solution was assayed as being 0.86 mg/ml. The solution was then diafiltered against 9 liters of NaCl-solution having a proportion of 2 mol/l. The diafilter used had a "cut off" at molecular weight 10 000. The aluminium proportions of the albumin solution and the permeate was assayed, after addition of given quantities of NaCl-solution. The results are set forth in the following Table 2.

Table 2

	Volume diafiltered	Albumin solution	Permeate
	solution, l	Al-cont. mg/ml	Al-cont. mg/ml
20	1.5	0.41	0.56
	3	0.32	0.31
	4.5	0.23	0.24
	6	0.16	0.16
25	9	0.09	0.10

The albumin solution was then diafiltered against 30 liters of distilled water for de-salting purposes, and the aluminium content of the solution was determined during the de-salting process. The results are set forth in the following Table 3:

Table 3:

	Volume, l	Albumin solution Al-cont, mg/ml
35	2	0.02

9

4	< 0.01
6	< 0.01
8	< 0.01
10	< 0.01

5

The solution was concentrated to an albumin content of 20%, after the de-salting process, whereafter the aluminium content was measured to 0.02 mg/ml.

10 Example 4:

41.4 kg of a 10-percent albumin solution was pH-adjusted to 7.0, and sodium chloride in solid form was added to a content of 2 mol/l. A sample of the solution was analyzed with respect to its contents of Al, Fe, Cr and Mg.

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The solution was diafiltered with 125 liters of sodium chloride solution having the content of 2 mol/l. The solution was then de-salted with distilled water until the sodium content was less than 0.7 mg/ml. This level was reached after adding 250 liters of distilled water.

20

After de-salting the solution, the solution was concentrated to an albumin content of 20% and sterile filtered and introduced into bottles (100 ml) for heat treatment at 60°C for 10 hours. The proportions in which the aforesaid metal were present in the solution were determined prior to the de-salting process and after heat-treating the bottles, the analysis results obtained being set forth in the following Table 4.

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30

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Table 4:

		mg/l			
		Al	Fe	Cr	Mg
5	Starting material calculated to 20% albumin	0.47	4.34	0.08	2.51
	Concentrate from dia-				
	filtration	0.02	0.7	0.03	0.1
	In bottles after heat				
	treatment	0.02	0.3	<0.01	0.1

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The present invention thus provides a simple and convenient method of removing undesirable multivalent metal ions bound to a protein. The method can be applied generally for cleansing proteins and is not restricted solely to the examples described in this document. It will also be seen that further variants and modifications of the invention are possible within the scope of the following claims. For instance, the proteins can be cleansed by ultrafiltration, although this method is not as rational as the described method, since it is then necessary to add further salt solution or water. The inventive principles remain unchanged, however.

25 Literature references:

1. Crapper D.R, Kishnan S S, Quittat S. Aluminium, neuro-fibrillary degeneration and Alzheimer's disease. Brain 1976, 99, 67-80.
- 30 2. Crapper D R, Quittat S, Krishnan S S et al.: Intracellular aluminium content in Alzheimer's disease, dialysis encephalo-Acta Neuropath 1980, 50, 19-24
- 35 3. Alfrey A C, Le Gendre G R, Kaehny W D: The dialysis encephalopathy syndrome. Possible aluminium

intoxication. N Eng. Med 1976, 294, 184-188.

4. Alfrey A C, Hegg A, Craswell P: Metabolism and toxicity of aluminium in renal failure. Am J Clin Nutr

5 1980, 33, 1509-1516

5. Per D P, Gajdusek D C, Garruto R M et al.: Intra-neuronal aluminium accumulation in amyothropic lateral sclerosis and Parkinson-dementia of Guam. Science 1982,

10 217, 1053-1055

6. May J C, Rains T C, Maienthal F J et al.: A survey of the concentrations of eleven metals in vaccins, allergenic extracts, toxoids, blood, blood derivatives, and other biological products. J Biol Stand 1986, 14, 363-375

Claims

1. A method of cleansing a protein from multivalent
5 metal ions bound thereto, c h a r a c t e r i z e d by
releasing the multivalent metal ions by substituting
said ions with monovalent metal ions, and then removing
said multivalent metal ions.
- 10 2. A method according to Claim 1, c h a r a c -
t e r i z e d by releasing and removing the multi-
valent metal ions, by subjecting the organic compound
with multivalent metal ions bound thereto to a diafil-
tration process against a solution which contains mono-
15 valent metal ions.
3. A method according to Claim 2, c h a r a c -
t e r i z e d by subjecting the organic compound,
subsequent to the exchange of multivalent metal ions
20 for monovalent metal ions, to renewed diafiltration
against a solution which essentially contains no metal
ions.
4. A method according to Claim 1, c h a r a c -
25 t e r i z e d by releasing and removing the multi-
valent metal ions by subjecting the organic compound
with multivalent metal ions bound thereto to a gel-
filtration process in a solution of monovalent metal
ions.
- 30 5. A method according to Claim 4, c h a r a c -
t e r i z e d by subjecting the organic compound,
subsequent to replacing the multivalent metal ions with
monovalent metal ions, to a renewed gel-filtration
35 process in a solution which essentially contains no

metal ions.

6. A method according to any one of Claims 1-5,
c h a r a c t e r i z e d in that the multivalent ions
5 consist of one or more of the metals aluminium, iron
and lead.

7. A method according to any one of Claims 1-6,
c h a r a c t e r i z e d by releasing and removing
10 the monovalent metal ions, subsequent to releasing and
removing the multivalent metal ions.

8. A method according to Claim 7, c h a r a c -
t e r i z e d in that the monovalent metal ions con-
15 sist of alkali metal ions or ammonium ions.

9. A method according to Claim 8, c h a r a c -
t e r i z e d in that the monovalent metal ions con-
sist of sodium, potassium or ammonium ions.

20 10. A method according to any one of Claims 1-9,
c h a r a c t e r i z e d by using the monovalent
metal ions in the form of an aqueous solution having a
content from about 0.15 M up to saturation content.

25 11. A method according to Claim 1, c h a r a c -
t e r i z e d in that the protein is albumin or gam-
maglobulin.

30 12. A method according to Claim 1, c h a r a c -
t e r i z e d in that the protein is albumin, and the
multivalent ions are aluminium ions.

[received by the International Bureau
on 29 October 1990 (29.10.90);

Original claims 1,2,4 and 8 replaced by new claim 1;
claims 3,5 and 7 replaced by new claim 2;
claims 6,9-12 replaced by new claims 3-7 (2 pages)]

1. A method of cleansing a protein from multivalent metal ions
5 bound thereto, characterized in that the multivalent metal ions
are released from the protein by substituting them with mono-
valent metal ions, consisting of alkali metal or ammonium ions,
by subjecting the protein with multivalent metal ions bound
thereto to a diafiltration process against a solution which
10 contains the monovalent metal ions, such that said multivalent
metal ions are displaced from the protein and are obtained in a
filtrate, or by subjecting the protein with multivalent metal
ions bound thereto to a gel filtration in a solution of the
monovalent metal ions, such that the multivalent metal ions are
15 displaced from the protein and are delayed in the filtration,
after which the multivalent metal ions released from the
protein are removed in a way known per se.
2. A method according to claim 1, characterized in that after
20 the substitution of the multivalent metal ions with the mono-
valent metal ions, said monovalent metal ions are removed from
the protein by subjecting said protein to a renewed diafiltra-
tion against a solution which essentially does not contain any
metal ions, or by subjecting said protein to a renewed gel
25 filtration in a solution which essentially does not contain any
metal ions.
3. A method according to claim 1 or 2, characterized in that
said multivalent metal ions consist of one or more of the
30 metal aluminum, iron and lead.
4. A method according to any of claims 1-3, characterized in
that said monovalent metal ions consist of sodium, potassium or
ammonium ions.
- 35 5. A method according to any of claims 1-4, characterized in
that said monovalent metal ions are used in the form of an
aqueous solution with a concentration from about 0.15 M up to
saturation.

6. A method according to claim 1, characterized in that the protein is albumin or gamma globulin.

- 5 7. A method according to claim 1, characterized in that the protein is albumin, and the multivalent metal ion is aluminum.

STATEMENT UNDER ARTICLE 19

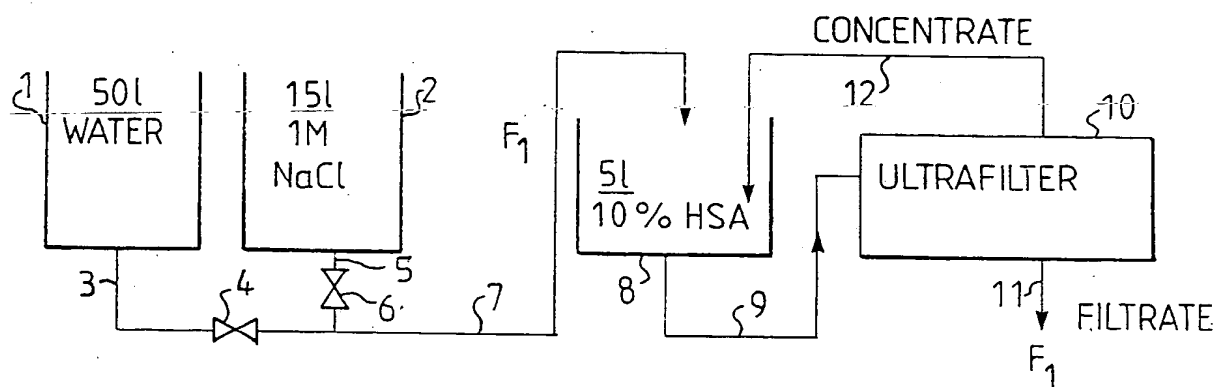
In the above application, we herewith file amended claims in duplicate under Article 19(1) PCT. The claims have been amended as follows:

The new claim 1 is a combination of the original claims 1, 2, 4 and 8. Furthermore, features have been inserted into the new claim 1 from the specification on page 3, line 27, to page 4, line 6, and page 4, lines 19 til 35. No new matter has been added.

The new claim 2 is a combination of the original claims 3, 5 and 7.


The new claims 3 to 7 are the same as the original claims 6 and 9 to 12, respectively, and only the claim numbers and the formal dependencies have been changed.

1/1



INTERNATIONAL SEARCH REPORT

International Application No PCT/SE 90/00442

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) ⁶ According to International Patent Classification (IPC) or to both National Classification and IPC IPC5: C 07 K 3/12		
II. FIELDS SEARCHED		
Minimum Documentation Searched ⁷		
Classification System	Classification Symbols	
IPC5	A 61 K; C 07 G; C 07 K	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in Fields Searched ⁸		
SE,DK,FI,NO classes as above		
III. DOCUMENTS CONSIDERED TO BE RELEVANT⁹		
Category [*]	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
X	US, A, 4256631 (NOBUO YOKOO ET AL.) 17 March 1981, see the whole document <div style="text-align: center;">--</div>	1-12
A	US, A, 4116948 (HELLMUT MITTENZWEI ET AL.) 26 September 1978, see the whole document <div style="text-align: center;">--</div> <div style="text-align: center;">-----</div>	1-12
<div style="display: flex; justify-content: space-between;"> <div style="width: 45%;"> <p>* Special categories of cited documents:¹⁰</p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> </div> <div style="width: 45%;"> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance, the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance, the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"&" document member of the same patent family</p> </div> </div>		
IV. CERTIFICATION		
Date of the Actual Completion of the International Search 19th September 1990	Date of Mailing of this International Search Report 1990 -09- 25	
International Searching Authority <div style="text-align: center;">SWEDISH PATENT OFFICE</div>	Signature of Authorized Officer <div style="text-align: center;">  Elisabeth Carlborg </div>	

**ANNEX TO THE INTERNATIONAL SEARCH REPORT
ON INTERNATIONAL PATENT APPLICATION NO. PCT/SE 90/00442**

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the Swedish Patent Office EDP file on **90-08-28**.
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Patent document cited in search report	Publication date	Patent family member(s)	Publication date	
US-A- 4256631	81-03-17	DE-A-C-	3010801	80-10-02
		FR-A-B-	2451745	80-10-17
		GB-A-B-	2044775	80-10-22
		JP-C-	1397692	87-09-07
		JP-A-	55124719	80-09-26
		JP-B-	62000885	87-01-10
		SE-A-	8002192	80-09-23

US-A- 4116948	78-09-26	AT-B-	344912	78-08-25
		DE-A-C-	2512936	76-09-30
		FR-A-B-	2305193	76-10-22
		GB-A-	1532713	78-11-22
		JP-C-	1309297	86-03-26
		JP-A-	51118809	76-10-19
		JP-B-	60032640	85-07-29

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